

①
Last time we arrived at 3 fundamental functions for a system with fixed V & N

entropy: $S(U, V, N)$ - U is controlled, this is maximized

energy: $U(S, V, N)$ - S is controlled, this is minimized

Helmholtz FE: $F(T, V, N)$ - T is controlled, this is minimized

(something else is always held fixed, ^{or controlled} and the state function of interest is maximized or minimized at equilibrium)

We need to define 2 more functions for more realistic lab conditions

Enthalpy

$$H(S, P, N) = U + PV$$

$$dH = dU + PdV + VdP$$

↑

we know this because $U(S, V, N)$

$$dU = TdS - PdV + \mu dN$$

$$\therefore dH = TdS - \cancel{PdV} + \mu dN + \cancel{PdV} + VdP$$

$$dH = TdS + VdP + \mu dN$$

This exact differential tells us a few things:

$H = H(S, P, N)$: S is controlled at boundaries, H is minimized

Also:

$$T = \left(\frac{\partial H}{\partial S} \right)_{P, N}$$

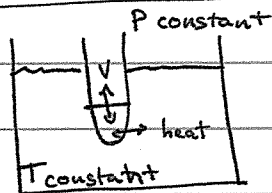
$$V = \left(\frac{\partial H}{\partial P} \right)_{S, N}$$

$$\mu = \left(\frac{\partial H}{\partial N} \right)_{S, P}$$

In general S is difficult to control, so we need:

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Gibbs Free Energy



← Pressure & Temperature are held constant, and Volume & Heat can change.

$$G \equiv H - TS \quad \text{or} \quad F + pV$$

$$dG = dH - TdS - SdT$$

↑

$$dH = TdS + VdP + \mu dN$$

$$dG = \cancel{TdS} + VdP + \mu dN - \cancel{TdS} - SdT$$

$$\therefore dG = -SdT + VdP + \mu dN$$

What we know

← natural variables are how we usually carry out experiments!

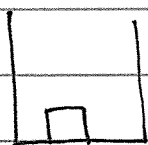
$$G = G(T, P, N)$$

$$-S = \left(\frac{\partial G}{\partial T} \right)_{P, N}$$

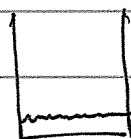
$$V = \left(\frac{\partial G}{\partial P} \right)_{T, N}$$

$$\mu = \left(\frac{\partial G}{\partial N} \right)_{P, T}$$

Consider Melting ice:



add
heat →



$T = \text{negligibly below } 0^\circ\text{C}$

G is at a minimum

$$= G_{\text{solid}}$$

$T = \text{negligibly above } 0^\circ\text{C}$

G is at a minimum

$$= G_{\text{liquid}}$$

What is $\Delta G = G_{\text{liquid}} - G_{\text{solid}}$

$$dP = 0$$

$$dN = 0$$

$$dT \approx 0$$

(ignore evaporation for now)

$\therefore dG = 0$ for the phase transition!

(3)

If $\Delta G = 0$ then $\Delta H = T_0 \Delta S$ ← phase trans. from temperature

The increase in entropy is balanced by an increase in enthalpy (weakened interactions)

Are these state functions: $U(T, V, N)$, $S(T, V, N)$,
useful? $H(T, P, N)$, $S(T, P, N)$

unnatural variables
for S

Consider:

$$F(T, V, N) = U(T, V, N) - TS(T, V, N)$$

minimizing $U(T, V, N)$ or maximizing $S(T, V, N)$ individually
 does not predict the state of equilibrium, but
 combining them to form F identifies an equilibrium
 if the constraints are T, V, N

We can measure $C_V(T)$ using a constant volume calorimeter

$$\Delta U = \int C_V(T) dT \quad \text{and} \quad \Delta S = \int \frac{C_V(T)}{T} dT$$

combine them to get:

$$F(T) = U(T) - TS(T)$$

Alternatively, under constant N, T, P conditions,
 $G(T, P)$ identifies the equilibrium state.

$$\begin{aligned} dH &= d(U + PV) = dU + P dV + V dP \\ &= \delta q + \delta w + P dV + V dP \end{aligned}$$

(4)

$$dH = \delta q + \underbrace{\delta w + PdV + VdP}_{=0 \text{ for a quasistatic process}} \quad \text{at constant } P$$

$$dH = \delta q \quad \text{at constant } P$$

$$C_p = \left(\frac{\delta q}{\delta T} \right)_p = \left(\frac{\partial H}{\partial T} \right)_p = T \left(\frac{\partial S}{\partial T} \right)_p$$

$$\text{So: } \Delta H(T, P) = \int_{T_A}^{T_B} C_p(T) dT$$

$$\Delta S(T, P) = \int_{T_A}^{T_B} \frac{C_p(T)}{T} dT$$

So, from a constant pressure calorimeter, we can get

$$G(T, P) = H(T, P) - TS(T, P)$$

The 3rd law of thermodynamics:

$$S(T) = \int_0^T \frac{C_v}{T'} dT' + S(0)$$

What is $S(0)$? The 3rd law defines $S(0) = 0$ for a pure perfectly crystalline substance @ $T = 0 \text{ K}$.

Let's do a few simple examples:

Equilibrium temperatures of objects in thermal contact:

object A

C_A, T_A

object B

C_B, T_B

We know that at equilibrium they'll both have the same T .

(5)

$$\Delta H = \Delta H_A + \Delta H_B = 0 \quad (\text{because we'll postulate that the objects are isolated from their surroundings})$$

$$\Delta H_A = \int_{T_A}^T C_A dT' = C_A (T - T_A) \quad \leftarrow \text{whatever final } T \text{ we get}$$

Likewise

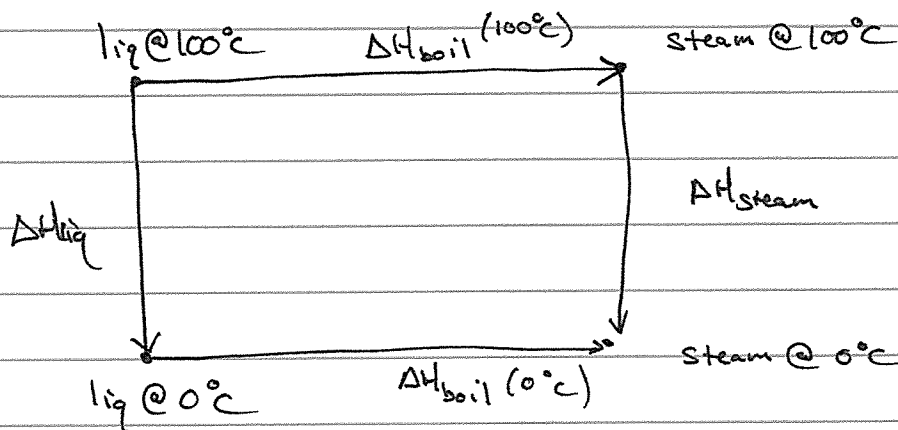
$$\Delta H_B = C_B (T - T_B)$$

$$C_A (T - T_A) + C_B (T - T_B) = 0$$

$$T = \frac{C_A T_A + C_B T_B}{C_A + C_B}$$

$$\text{if } C_A = C_B \Rightarrow T = \frac{T_A + T_B}{2}$$

Another example: Use Thermodynamic cycles to determine hard to measure quantities.



$$\Delta H_{\text{boil}}(100^\circ\text{C}) = 540 \frac{\text{cal}}{\text{g}}$$

$$C_{P,l} = 1.00 \frac{\text{cal}}{\text{kg}}$$

$$C_{P,\text{steam}} = 0.448 \frac{\text{cal}}{\text{kg}}$$

$$\Delta H_{\text{liq}} = \int_{100}^0 C_{P,\text{liq}} dT = -100 \text{ cal g}^{-1}$$

$$\Delta H_{\text{steam}} = \int_{100}^0 C_{P,\text{steam}} dT = -44.8 \text{ cal g}^{-1}$$

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$$\Delta H_{\text{boil}}(0^\circ\text{C}) = \Delta H_{\text{boil}}(100^\circ\text{C}) - \Delta H_{\text{liq}} + \Delta H_{\text{steam}}$$

$$= (540 + 100 - 44.8) \text{ cal g}^{-1} =$$

$$= 595.2 \frac{\text{cal}}{\text{g}}$$