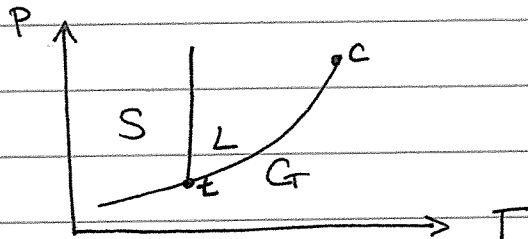


Phase Equilibria

①

A brief review of phase diagrams:



← The standard solid-liquid-gas behavior of most substances.

E = the triple point
where all 3 phases coexist

Water looks a bit different.
The slope of the S/L
coexistence line goes to the
upper left.

at this one point there are no thermodynamic
"degrees of freedom" (P & T have been specified).

In the solid, liquid & gas regions there are 2 degrees
of freedom (we can change P or T without changing
phase)

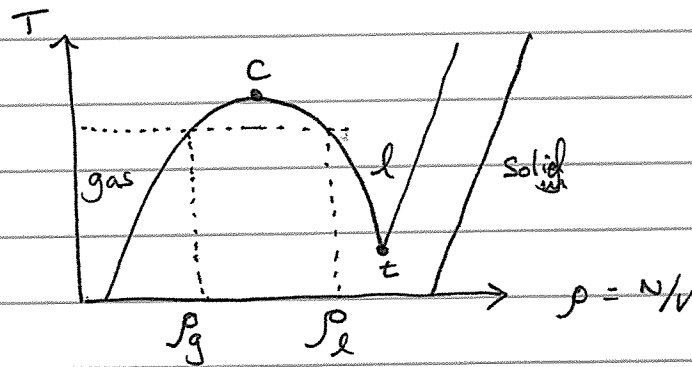
Along a coexistence line between 2 phases, we say there
is one degree of freedom (if we change P , we must
also change T to stay on the line).

The Gibbs phase rule: $f = 3 - p$
↑ # of coexisting phases
degrees of freedom

Critical Points

(2)

Another way of viewing the same phase diagram



← An "orthobaric" density plot

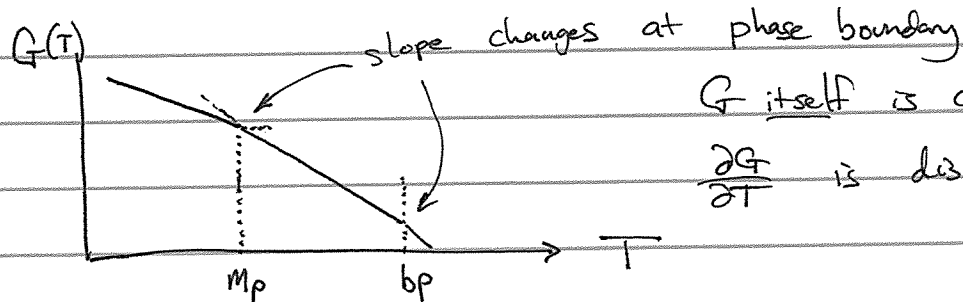
At any temperature, we can read across to the densities of the liquid & gas that are at equilibrium

Note that the densities of these coalesce at the critical point.

At the critical point, all sorts of strange things happen:

- 1) Density fluctuations occur at all length scales, so
- 2) incoming light is scattered (critical opalescence)
- 3) $\Delta S_{\text{vaporization}} = \frac{\Delta H_{\text{vap}}}{T}$ and both $\rightarrow 0$ at the critical point.

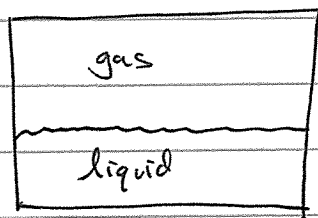
The Gibbs Free energy is closely tied to the phase diagram



G itself is continuous, but $\frac{\partial G}{\partial T}$ is discontinuous

Chemical Potentials

(3)



← if we're at the boiling point these phases are in equilibrium

$$G = G^l + G^g$$

if n moles of molecules move from one phase to the other:

$$dG = \left(\frac{\partial G^l}{\partial n^l} \right) dn^l + \left(\frac{\partial G}{\partial n^g} \right) dn^g$$

but, $dn^l = -dn^g$

$$\therefore dG = \left[\left(\frac{\partial G}{\partial n^g} \right)_{P,T} - \left(\frac{\partial G}{\partial n^l} \right)_{P,T} \right] dn^g$$

$$dG = \left[\overset{\nearrow}{\mu_g} - \overset{\nearrow}{\mu_l} \right] dn^g$$

← chemical potentials

At equilibrium $dG=0$, but dn^g isn't zero because molecules are constantly shuttling back & forth, so

$$\mu_g = \mu_l \quad \text{at equilibrium coexistence}$$

In general $\mu_\alpha \equiv \left(\frac{\partial G}{\partial n_\alpha} \right)_{T,P}$

$$\mu_\alpha(T,P) = \mu_\beta(T,P) \quad \text{at equilibrium}$$

Take derivatives of both sides:

$$\left(\frac{\partial \mu_\alpha}{\partial T} \right)_P dT + \left(\frac{\partial \mu_\alpha}{\partial P} \right)_T dP = \left(\frac{\partial \mu_\beta}{\partial T} \right)_P dT + \left(\frac{\partial \mu_\beta}{\partial P} \right)_T dP$$

remember that μ_α is just the Gibbs free energy/mole, so,

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$$\left(\frac{\partial \mu_\alpha}{\partial P}\right)_T = \frac{1}{n_\alpha} \left(\frac{\partial G_\alpha}{\partial P}\right)_T = \frac{1}{n_\alpha} V_\alpha = \text{molar volume of } \alpha$$

$$\left(\frac{\partial \mu_\alpha}{\partial T}\right)_P = \frac{1}{n_\alpha} \left(\frac{\partial G_\alpha}{\partial T}\right)_P = \frac{1}{n_\alpha} (-S_\alpha) = \text{molar entropy of } \alpha$$

So we have:

$$V_\alpha dP - S_\alpha dT = V_\beta dP - S_\beta dT$$

$$\therefore \frac{dP}{dT} = \frac{S_\beta - S_\alpha}{V_\beta - V_\alpha} = \frac{\Delta S}{\Delta V}$$

Now, at equilibrium, $\Delta G = \Delta H - T\Delta S = 0$, so $\Delta S = \frac{\Delta H}{T}$

$$\therefore \frac{dP}{dT} = \frac{\Delta H_{\text{vap}}}{T\Delta V}$$

↗ change in pressure as we move along the
vapor-liquid coexistence line

This is called the Clapeyron equation and gives
us the slope of 1-line in the phase diagram

There's a cool modification of this:

$$\Delta V = V_g - V_l \leftarrow \text{molar volumes}$$

↗ much larger than V_l

$$\therefore \frac{dP}{dT} \approx \frac{\Delta H_{\text{vap}}}{TV_g} \leftarrow V_g \approx \frac{n_g RT}{P} = \frac{RT}{P}$$

$$\therefore \frac{1}{P} \frac{dP}{dT} = \frac{\Delta H_{\text{vap}}}{RT^2} \Rightarrow \boxed{\frac{d \ln P}{dT} = \frac{\Delta H_{\text{vap}}}{RT^2}}$$

↗ Clausius-Clapeyron!

The integrated form of Clausius - Clapeyron:

(5)

$$\ln \frac{P_2}{P_1} = \frac{\Delta H_{\text{vap}}}{R} \left(\frac{T_2 - T_1}{T_1 T_2} \right)$$

← relationship between
vapor pressures
 P_1 & P_2 at

2 different temperatures

↗
Super important in industrial processes & distillation...

Chemical potentials & Statistical Mechanics

Some more details on μ :

$$\mu = \left(\frac{\partial G}{\partial n} \right)_{T,P} = \left(\frac{\partial A}{\partial n} \right)_{T,V}$$

but:

$$A = -k_B T \ln Q \quad \leftarrow \text{Partition Function}$$

$$\mu = -k_B T \left(\frac{\partial \ln Q}{\partial n} \right) = -RT \left(\frac{\partial \ln Q}{\partial N} \right)$$

But: $Q = \frac{q^N}{N!} \quad \leftarrow \text{molecular p.f.}$

$$\ln Q = N \ln q - N \ln N + N$$

$$\frac{\partial \ln Q}{\partial N} = \ln q - \ln N - 1 + 1 = \ln \frac{q}{N}$$

$$\therefore \mu = -RT \ln \left(\frac{q}{N} \right)$$

for an ideal gas, $q = \left(\frac{2\pi m k_B T}{h^2} \right)^{3/2} V$

$$\frac{q}{N} = \frac{q}{V} \cdot \frac{V}{N} = \left(\frac{2\pi m k_B T}{h^2} \right)^{3/2} \frac{RT}{P}$$

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$$\mu = -RT \ln \left[\frac{q}{V} \frac{k_B T}{P} \right]$$

$$\mu = -RT \ln \left(\frac{q}{V} k_B T \right) + RT \ln P$$

$$\mu(T, P) = \underbrace{\mu_0(T)}_{\substack{\text{standard state} \\ \text{chemical potential}}} + RT \ln \frac{P}{P_0} \quad \leftarrow \begin{array}{l} \text{deviations} \\ \text{from standard} \\ \text{state} \end{array}$$

(using a molecular partition function
at standard conditions)